



## **Shaping the future: renewable fuels and chemicals from solar energy for a climate-neutral Europe**

Joint roadmapping workshop on future milestones by  
SUNERGY, EIC and DG RTD

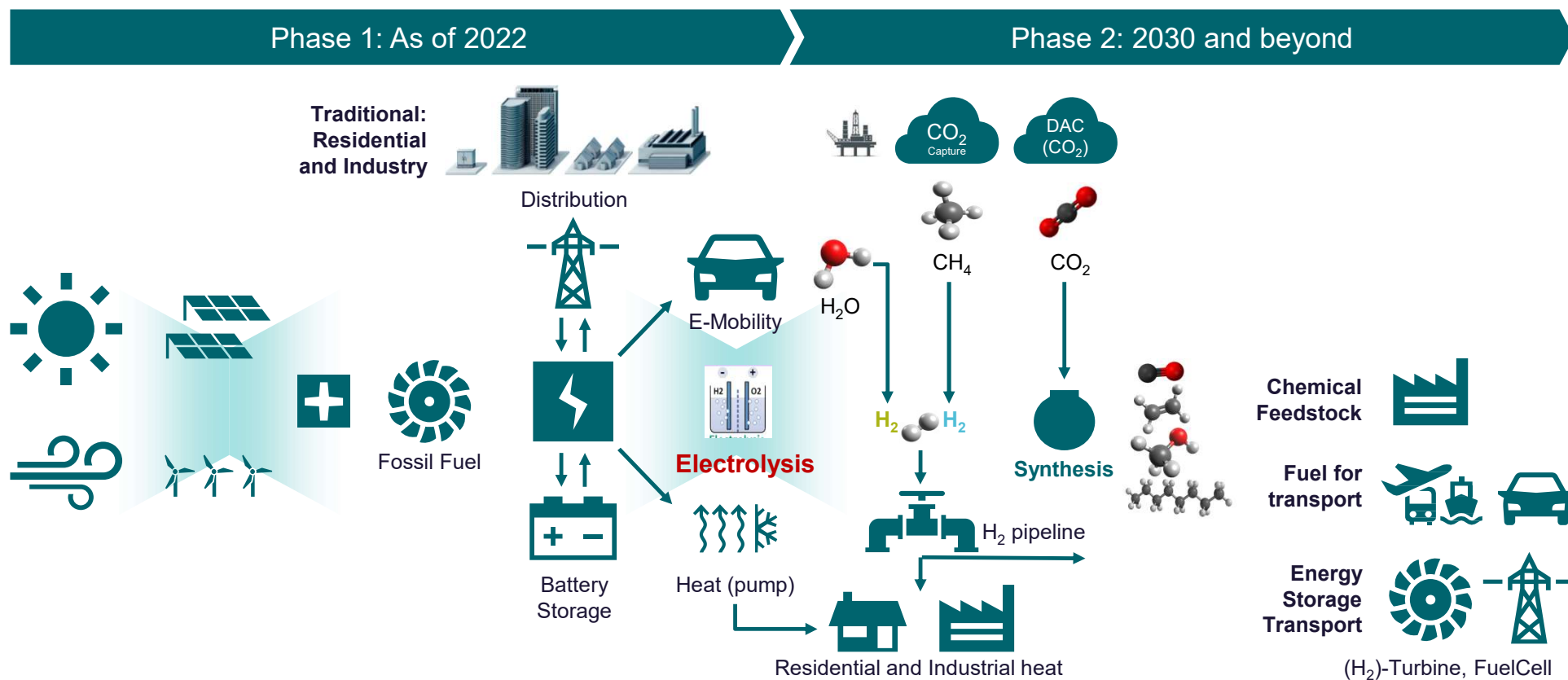
Brussels, 14/15 June 2022

## **The future of electrolyzer for the new energy system: The importance of integration**

Max Fleischer

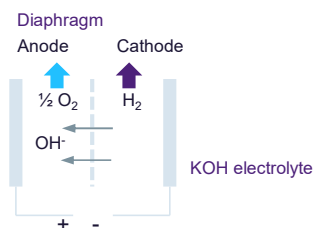


# As Siemens Energy, we believe in an accelerating transition towards a sustainable and decarbonized energy world

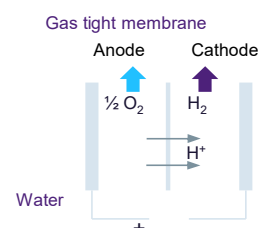


## There are three considerable technologies of water electrolysis differing in their characteristics.

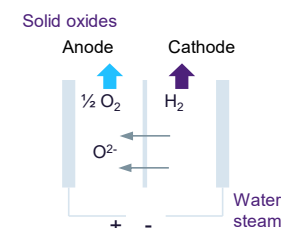
### Alkaline Electrolysis



### PEM Electrolysis



### High temperature



Electrolyte	KOH <sup>3</sup>	Polymer membrane	Ceramic membrane
Circulated medium	KOH <sup>3</sup>	Water	Steam
Operational temperature <sup>1</sup>	60 – 90 °C	RT <sup>4</sup> – 80 °C	700 – 900 °C
Technical maturity <sup>1</sup>	Industrially mature	Industrially mature	Lab/demo
Field experience <sup>1</sup>	●	●	●
Cold start capability <sup>2</sup>	●	●	●
Intermittent operation <sup>2</sup>	●	●	●
Scalability up to multi Giga Watt <sup>2</sup>	●	●	●
Reverse (fuel cell) mode <sup>1</sup>	●	●	●

● Existing/available    ● In development/limited    ● Not possible, not available

Source: 1 Fraunhofer | 2 IndWede | 3 KOH: Potassium hydroxide | 4 Room temperature

# Given the Volatility of Renewable Input, The Hydrogen Production needs to be Agile

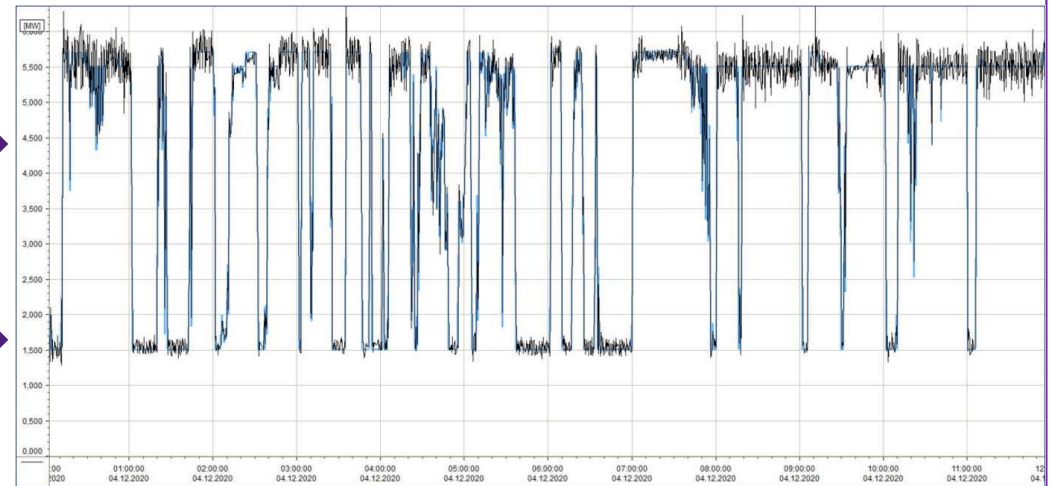
## Infinitely variable plant operation

- Power controlled operation based on real power price with 15 min time frames (see example on right side)
- Dynamics: maximal ramp rate in array 10% per second power change possible
- Always fast ramp-up

## Real plant data from an exemplary H2 Sielyzer

Target power selection

Power consumption electrolyzer

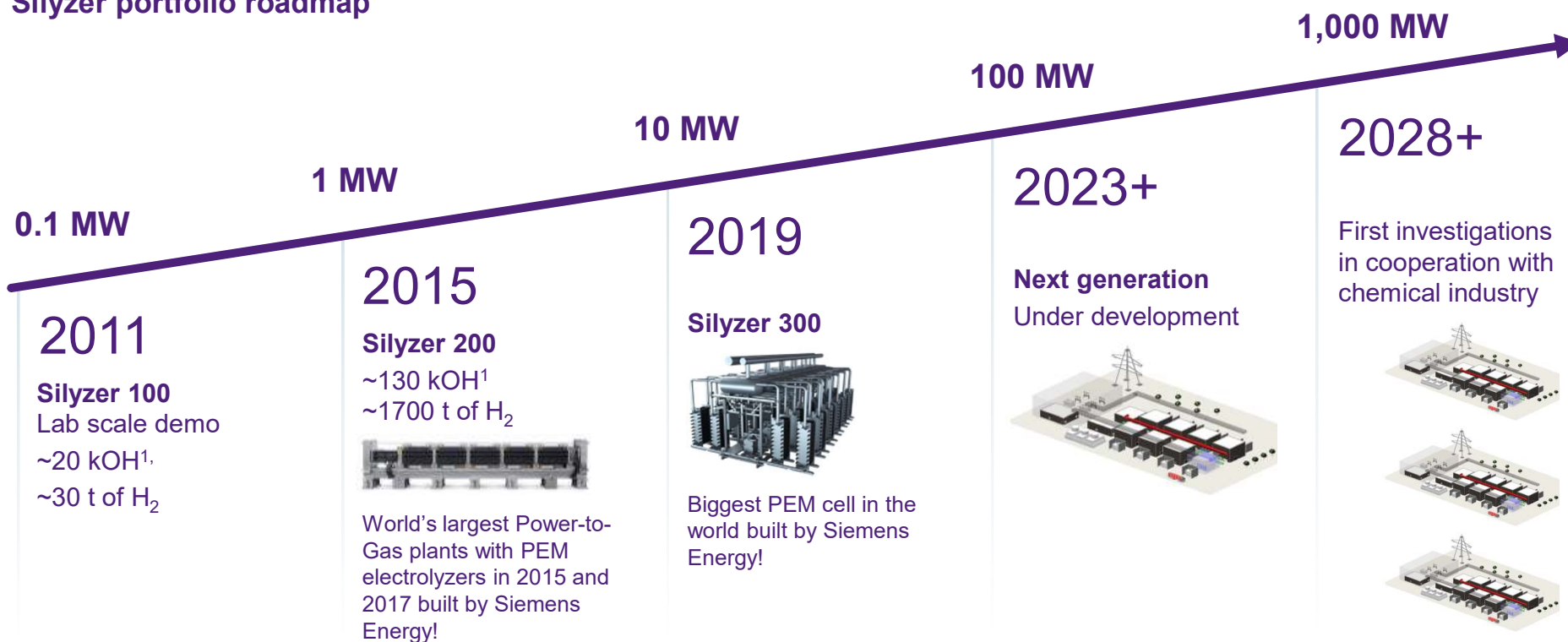


— Operating

— Set point

# Silyzer portfolio scales up by factor 10 every 4 – 5 years driven by market demand and co-developed with our customers

## Silyzer portfolio roadmap



<sup>1</sup> 1000 accumulated Operating Hours; Data OH & tons as of Oct 2020

## Silyzer 300 – Full Module Array

The next paradigm in PEM electrolysis

Silyzer 300 – full module array (24 modules)



**17.5 MW**  
plant power demand

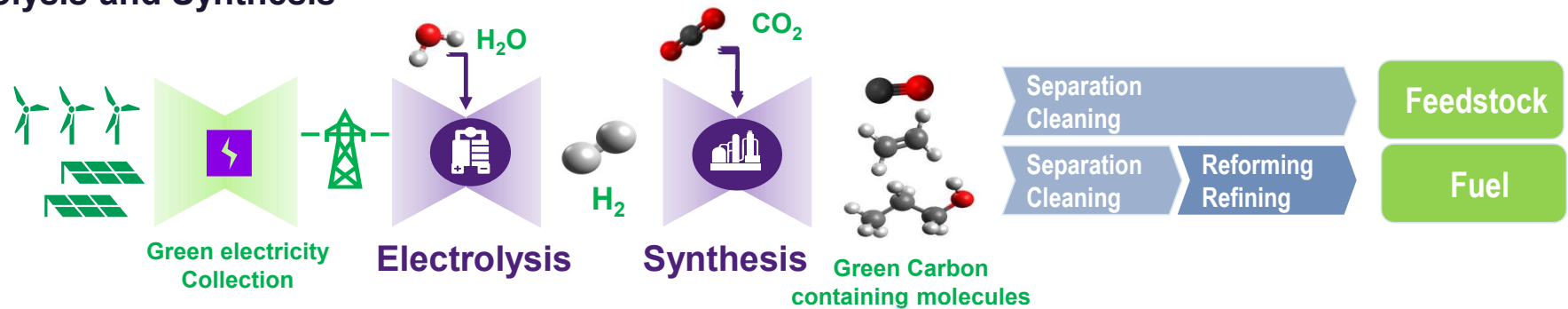
**> 75.5 %**  
plant efficiency

**24 modules**  
to build a full module  
array

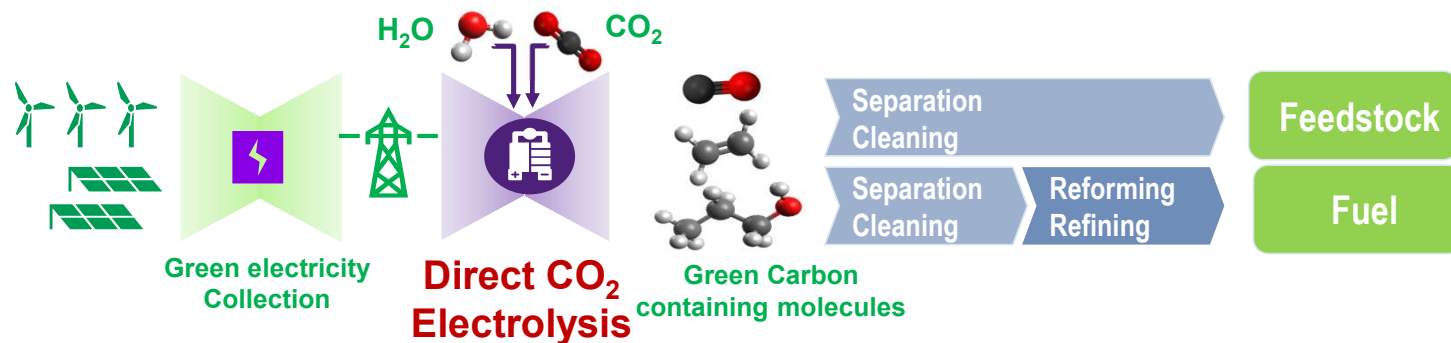
**335 kg**  
hydrogen per hour

# Simplifying the Process Chain: New Process to get to Green Hydrocarbons:

The conventional route via green hydrogen uses two different main conversion steps:  
**Electrolysis and Synthesis**

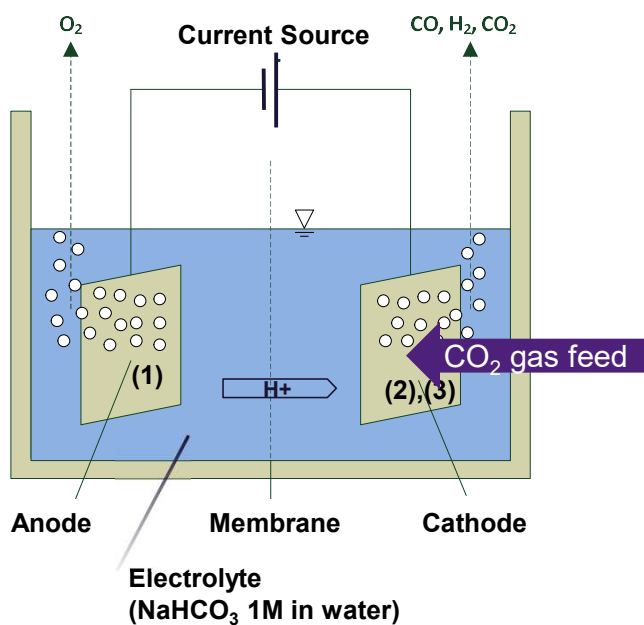


Our new and simpler route: **Direct Electrochemical Conversion of  $CO_2$**  by one conversion step



# Base Idea: A Novel Type of Electrolyzer is fed with CO<sub>2</sub> and H<sub>2</sub>O at ambient conditions and directly reduces CO<sub>2</sub> .

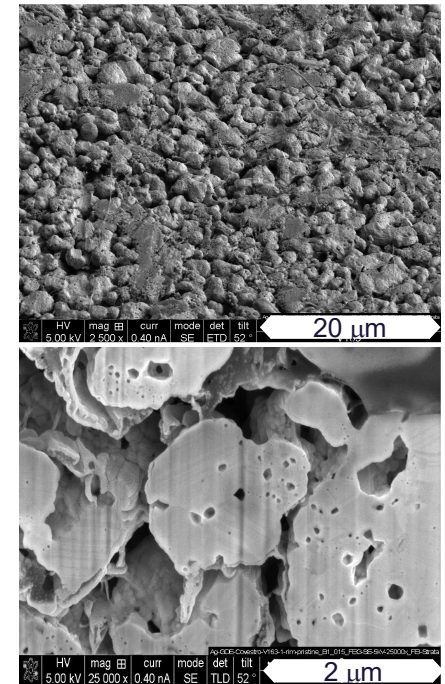
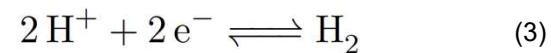
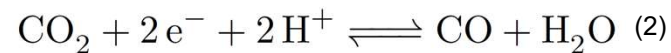
Anode material: Platinum, Cathode material : Silver porous



**Anode Reaction:**



**Cathode Reaction:**



Top view and cross section of silver catalyst

P. Jeanty, E. Magori, M. Fleischer, O. Hinrichsen, K. Wiesner-Fleischer, C. Scherer, *Journal of CO<sub>2</sub> Utilization* 24 (2018) 454-462



# What products can be made directly out of CO<sub>2</sub> and H<sub>2</sub>O?

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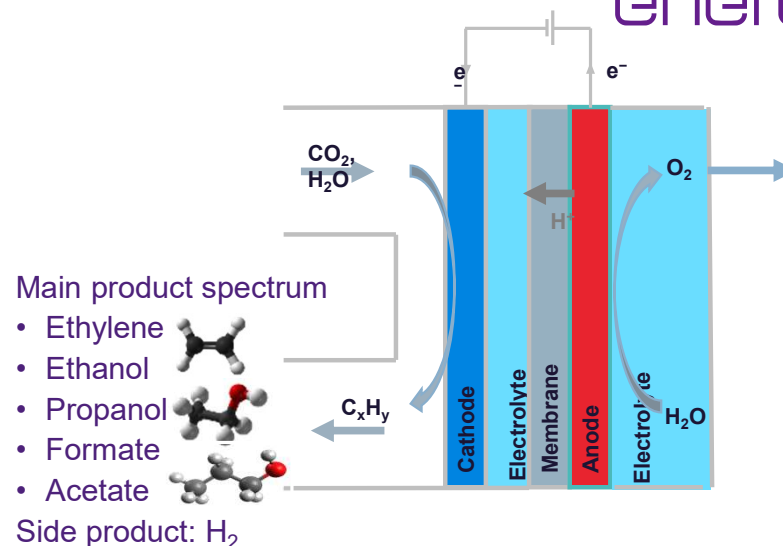
## Products using gas diffusion-based CO<sub>2</sub> electrolyzers

**Silver catalyst based:** stable catalyst, upscale of electrolyzer stack

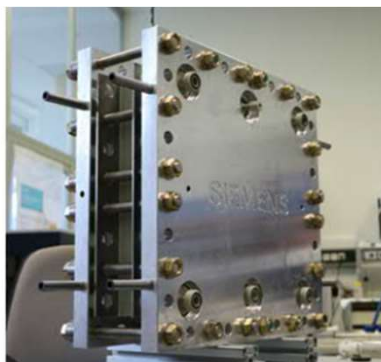
- Production of **CO** (>95%) for local CO supply
- Production of **CO / H<sub>2</sub> mixtures (Syngas)** for chemical synthesis – Fischer Tropsch process for hydrocarbons.

**Copper catalyst based:** stable catalyst in development\*, include this catalyst in CO-stack

- Target: **Ethylene** production for chemical production
- Target: Mix of **C2/C3 components (Ethanol, Ethylene, Propanol)** selectivity > 75% + CO/H<sub>2</sub> as green fuel precursor



Scale-up for CO (**Rheticus**)  
10 cell stack of 300cm<sup>2</sup> cell



Scale up for CO (**Kopernikus**)  
5000cm<sup>2</sup> cell



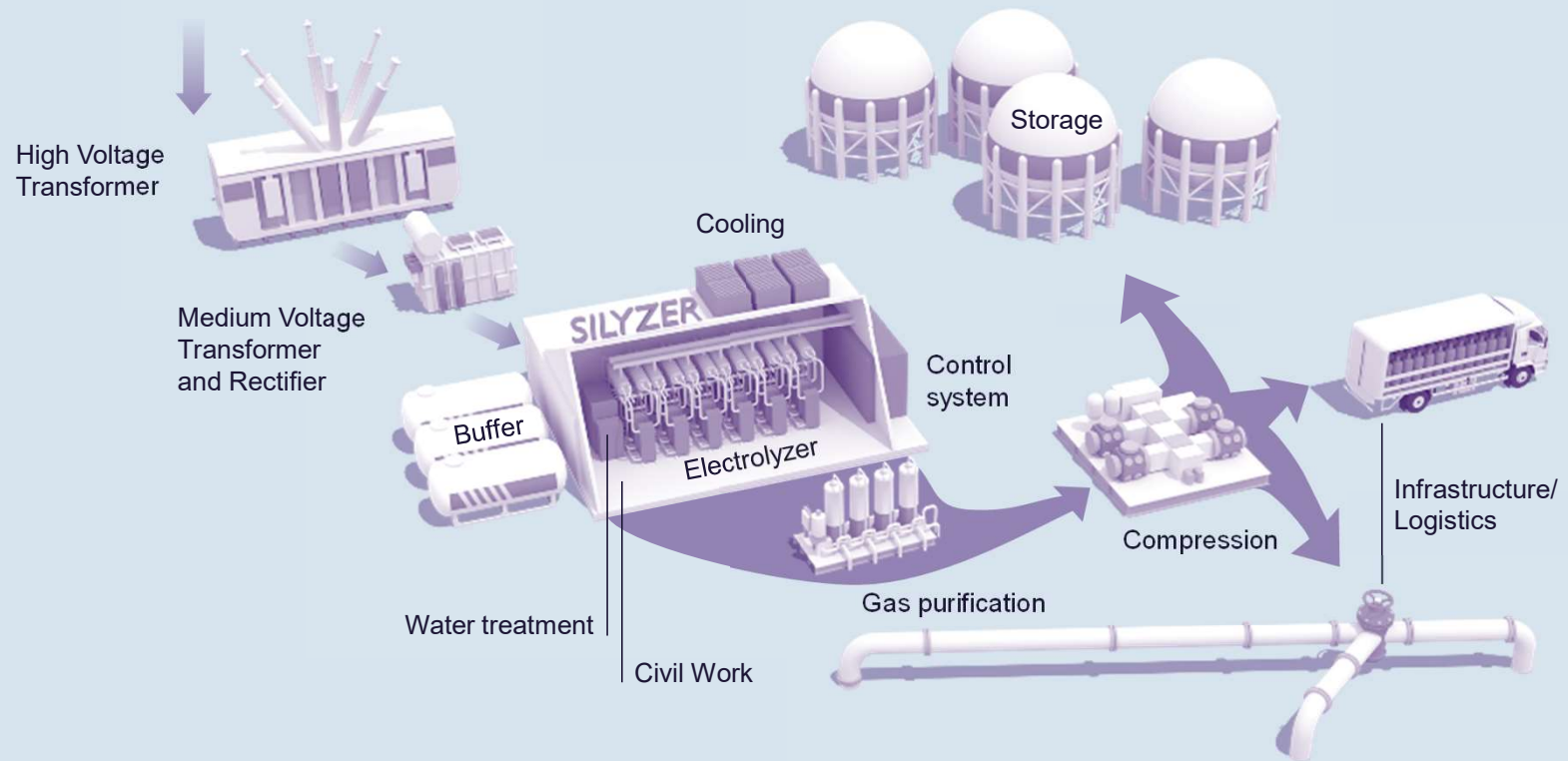
\* In lab devices:  
several 100hs of stability

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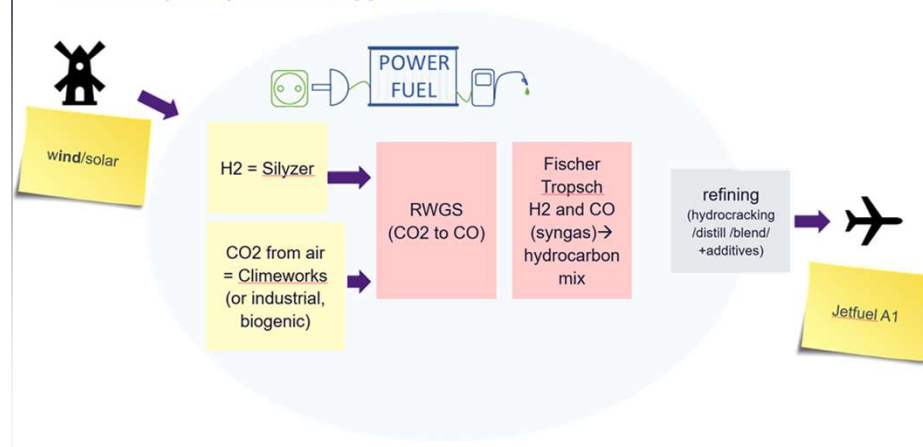
# Industrialized Electrolysis is more than just an electrolyzer



# Water electrolysis directly connected to renewables in island mode: Economic operation (e.g. PV) leads to significant no load periods of electrolyzer

**POWERFUEL German** funded simulation project for the  
Generation of SAF (Jet Fuel)

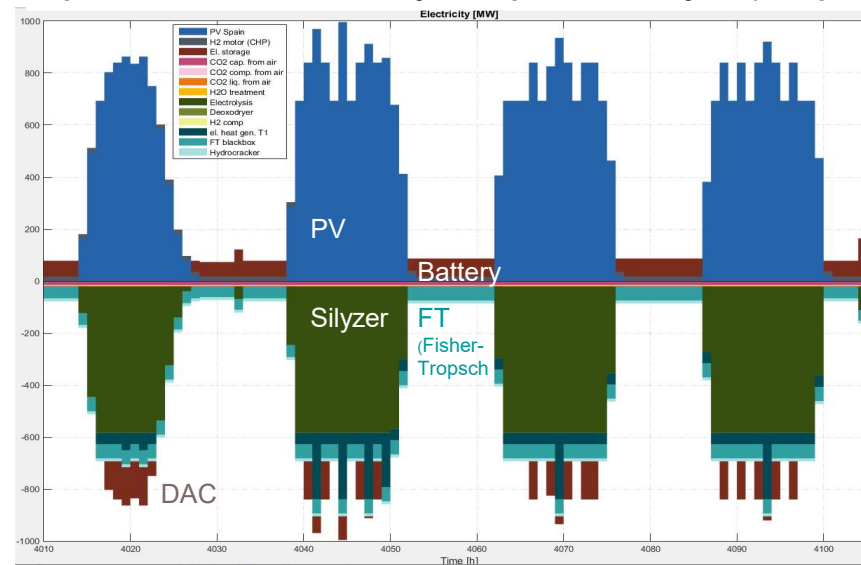
short scope of powerfuel approach



Simulation Scenario:  
Separate consideration Wind(various) /PV(Spain) + Battery, Electrolysis, DAC,  
RWGS, FT Synthesis, Refining → cost of Jet Fuel mimimized

Today's cost optimum of overall CAPEX vs. electricity costs is agile electrolyzer operation with no buffering by batteries

Operation scheme of 100 MW jet fuel plant driven by PV (200t per day)



\*Battery buffering of electrolysis not economic.  
Batteries only used for buffering of synthesis

# Water electrolysis connected to grids: Economic operation requires steep load ramps and complete turn-off

## Wind<sub>2</sub>Hydrogen onshore

(OMV: Funded H<sub>2</sub> production with grid connection)

<https://www.energy-innovation-austria.at/article/wind2hydrogen-w2h/>

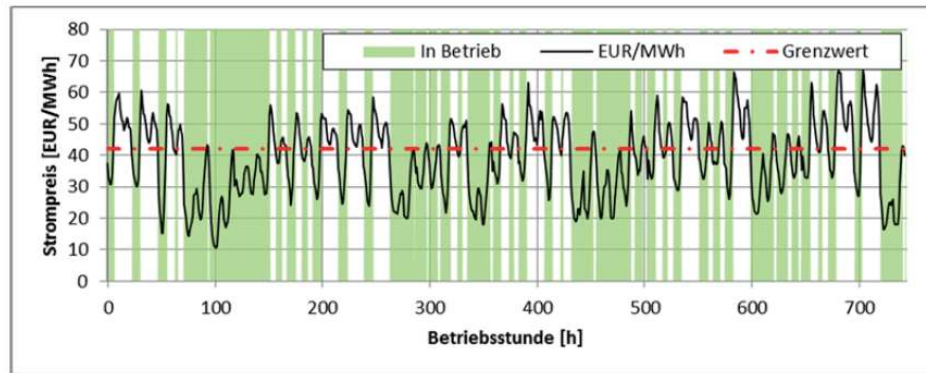


Abbildung 6: Betriebsweise mit Strompreis als Führungsgröße; die grün markierten Bereiche stellen die Betriebszeiten des Elektrolysesystems dar; Strompreisverlauf aus [4]

Electrolyzer operates only in times with positive business case (i.e. high portion of fluctuating renewables)

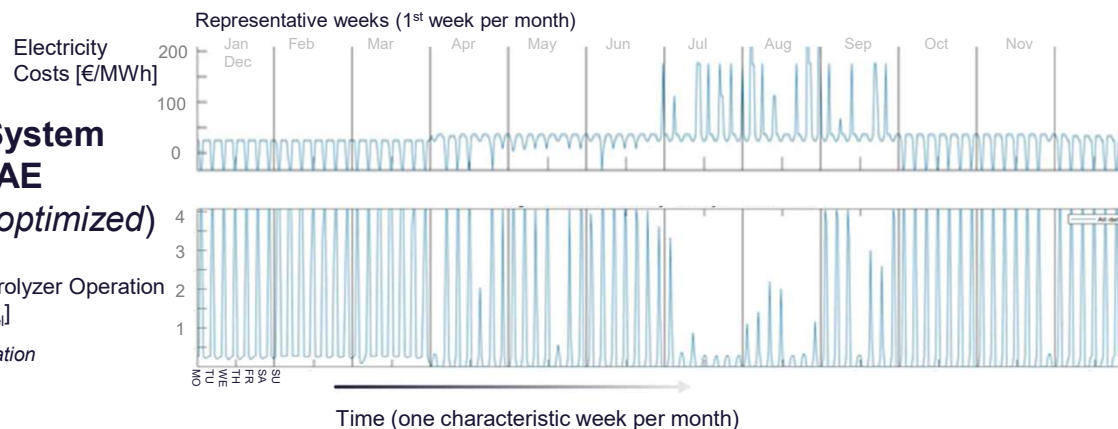
Similar: **Audi eGas plant Werlte**



Green CNG for passenger cars 2013-2021

## SE Energy System Modelling UAE (overall cost optimized)

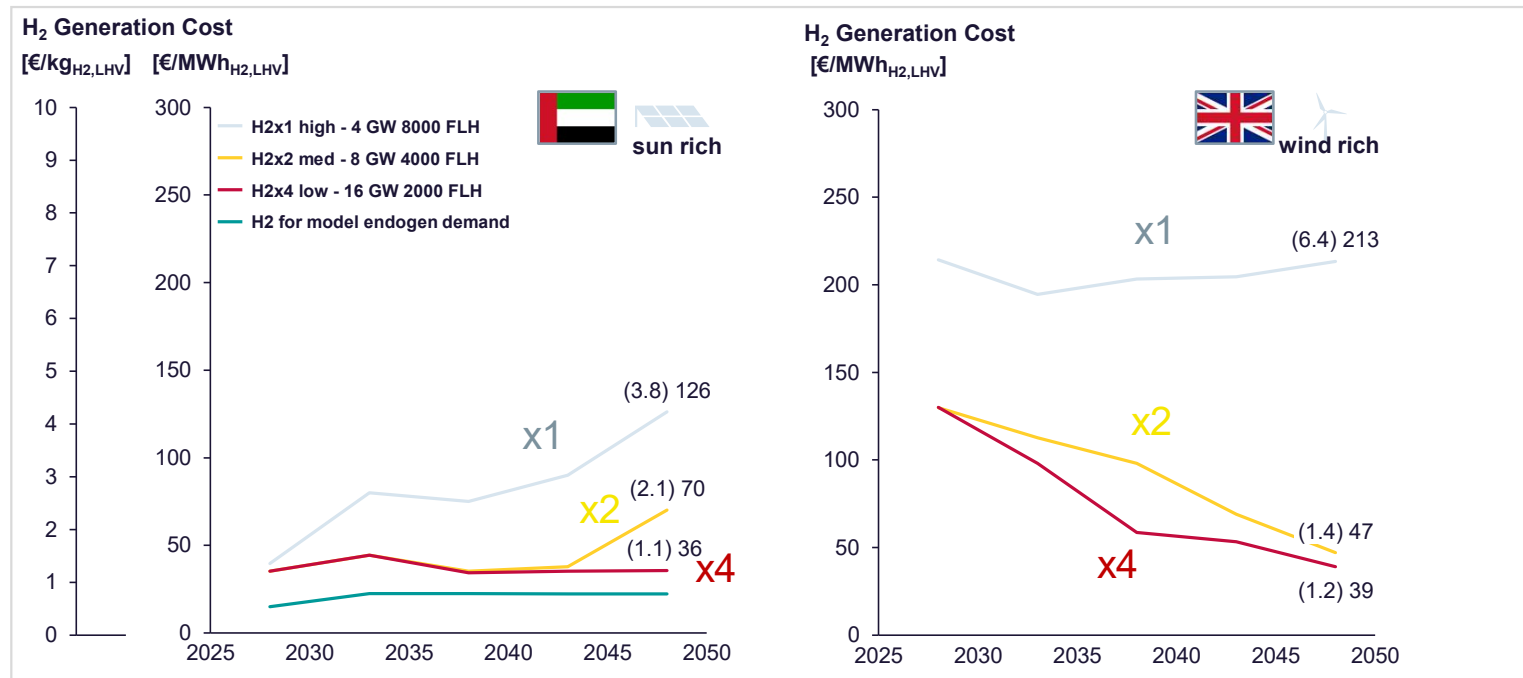
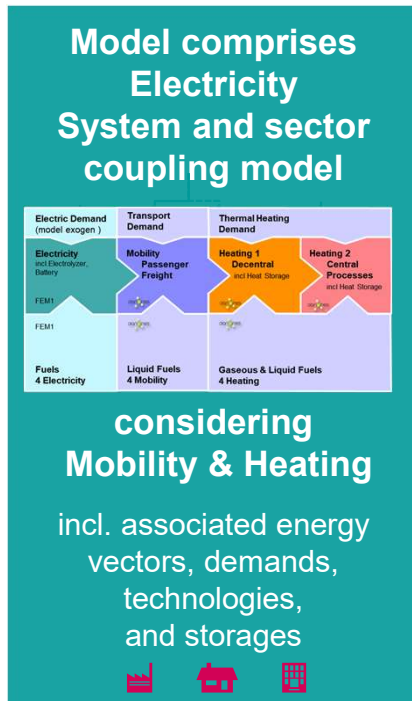
Source: SE owned simulation



The cost optimum of electrolyzer CAPEX vs. electricity costs requires agile electrolyzer operation

# Energy System Modelling on National Level: Comparing a Sun rich (UAE) and a Wind rich (UK) country to determine green H<sub>2</sub> production costs.

Compared to UK, H<sub>2</sub> production prices in UAE are usually lower – overbuilding can reduce generation costs



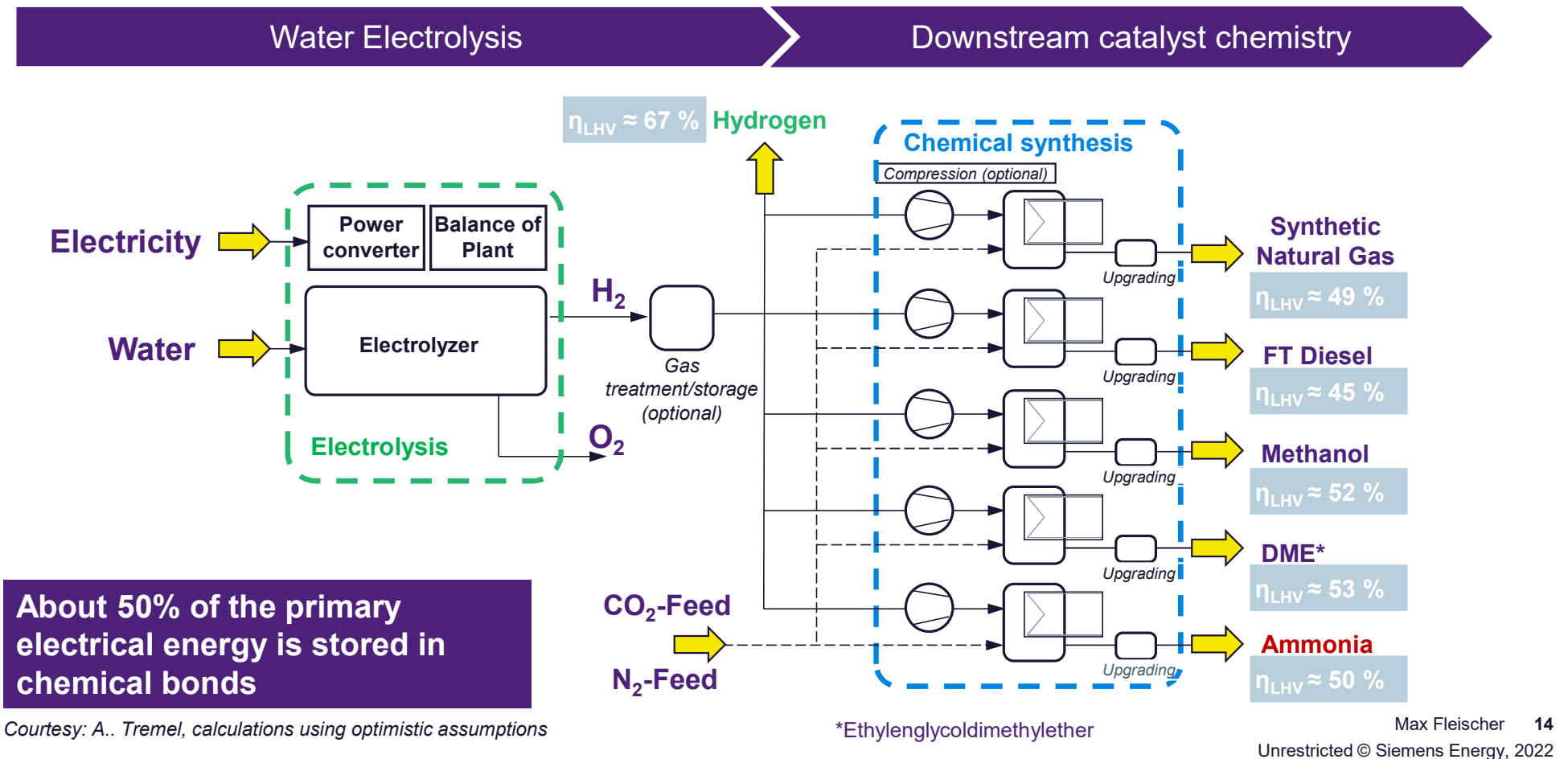
Overbuilding of Electrolyzer capacity compared to export target:

x1 x2 x4

allows to use temporarily cheap electricity

Source: SE owned simulation

# The conversion efficiency over the whole value chain including with Downstream Synthesis to Fuel needs to be optimized?





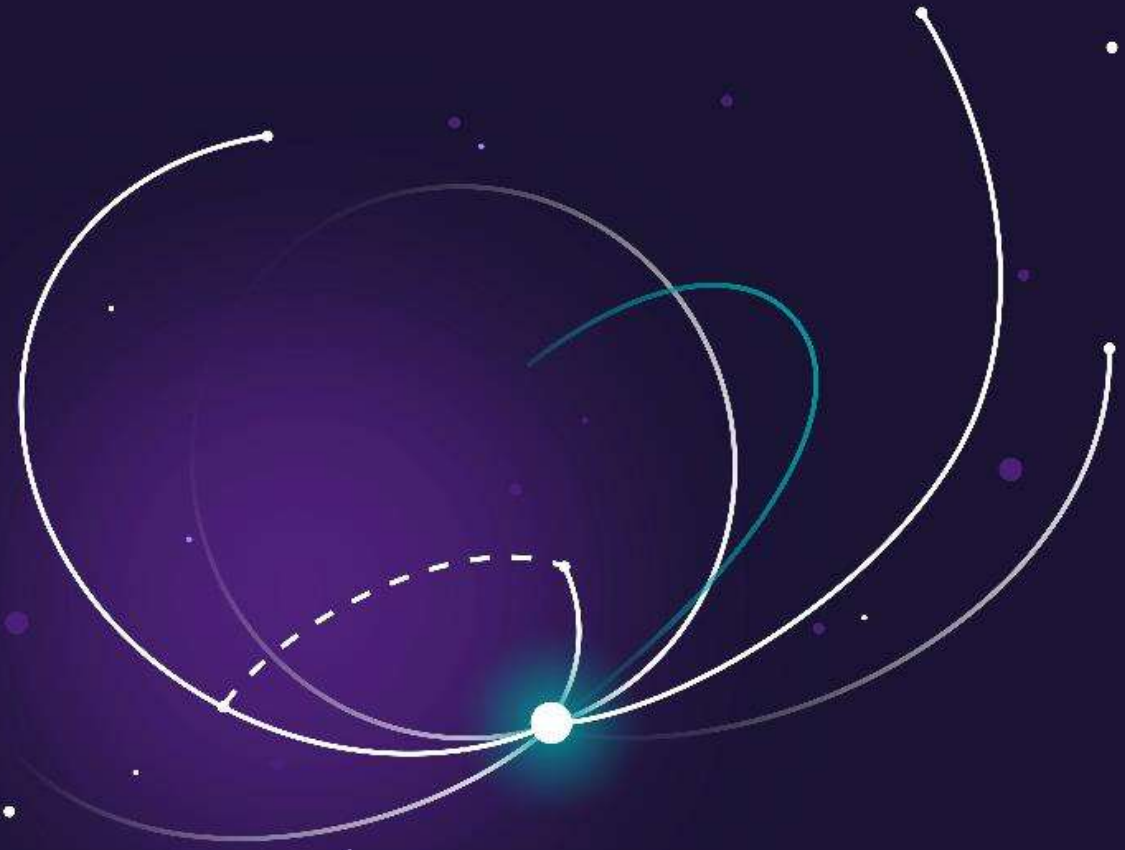
**Thank you for your time!**

**SIEMENS**  
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# Energy densities in storage:

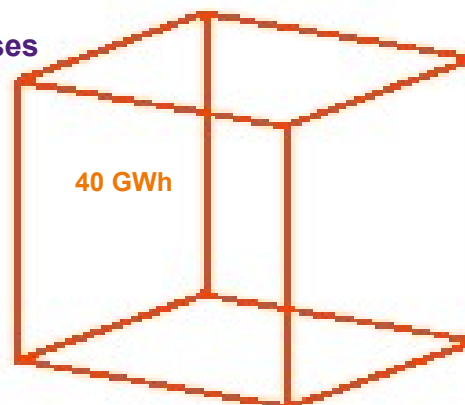
## Chemical storage (green fuel) shows the Utmost Energy Density for long-term energy storage and transport

9 pumped Hydro Power Plants in Germany can store 40 GWh with gravimetric storage



Footprint for storage of 40 GWh in chemical bonds

Gases



166 m: Methane, 1 bar  
230 m: Hydrogen, 1 bar

Compressed Gas  
Batteries



50 m: Lithium-ion batt.  
40 m: Hydrogen, 200 bar

Liquid Fuel



16 m: Diesel  
20 m: Methanol  
18 m: Ethanol



# Given the Volatility of Renewable Input, the Production along the Whole Value Chain needs to be Optimized and Buffered

Overview on hydrogen economy (schematic)

